Theory of the nonsteady diffusion growth of a gas bubble in a supersaturated solution of gas in liquid

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Abstract

Using a self-similar approach a general nonsteady theory is elaborated for the case of the diffusion growth of a gas bubble in a supersaturated solution of gas in liquid. Due to the fact that the solution and the bubble in it are physically isolated, the self-similar approach accounts for the balance of the number of gas molecules in the solution and in the bubble that expells incompressible liquid solvent while growing. The rate of growth of the bubble radius in its dependence from gas solubility and solution supersaturation is obtained. There is a nonsteady effect of rapid increase of the rate of bubble growth simultaneous with the growth of the product of gas solubility and solution supersaturation. This product is supplied with a limitation from above, which also stipulates isothermal conditions of bubble growth. The smallness of gas solubility is not presupposed.

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Introduction

The basis of the study of the diffusion growth of a gas bubble in a supersaturated solution of gas in liquid is usually [1, 2, 3, 4, 5, 6] founded on a steady solution of the diffusion equation of gas molecules in liquid. It is the purpose of this paper to elaborate a general nonsteady theory for the diffusion growth of a gas bubble in a supersaturated solution of gas in liquid, exploiting a self-similar approach elaborated in [7] by the example of the diffusion growth of a liquid droplet in a supersaturated vapor-gas mixture. This theory does not exploit the supposition that the concentration profile of gas dissolved around the growing bubble is steady.

The object under consideration is a liquid solution of gas which includes a gas bubble of the same single-component substance that is dissolved in the liquid. We shall consider the volume of the solution to be so large that heterogeneous nucleation of bubbles at its boundaries does not influence the volume of the solution where the bubble is located. The bubble is rather large, which makes it possible to neglect the Laplace forces. The solution is presupposed to be diluted, while the gas in the bubble – perfect. Dissociation and chemical transformations of the dissolved molecules are also neglected. Due to high heat conductivity of the liquid solution, we shall consider all the system of the solution and of the bubble as having the same temperature. Temperature and pressure in the solution are given. The solubility of gas in liquid is traditionally seen as a dimensionless value defined (at given temperature and pressure) as the ratio between the volume of gas and the volume of liquid dissolved in this gas.

We shall study a realistic situation when the diffusion of molecules of the dissolved gas in the presence of a bubble occurs simultaneously with the motion of the liquid solvent which is caused by the movement of the bubble surface and due to the solvent incompressibility. This problem has not been studied in [1, 2, 3, 4, 5, 6]. Taking into account the fact that the solution and the bubble in it are physically isolated, we shall consider the balance of the number of gas molecules in the solution and in the bubble that expells the incompressible liquid solvent while growing. Using the self-similar theory as a basis, we shall derive an equation for the rate of growth of the bubble radius in its dependence on gas solubility and solution supersaturation. We shall describe a significantly nonsteady effect of a rapid increase of the rate of bubble growth at the increase of the product of gas solubility and

solution supersaturation. This product will be provided with the limitation from above, which stipulates the isothermal conditions of bubble growth. The smallness of gas solubility will not be presupposed.

I. GAS BUBBLE GROWING IN LIQUID SOLUTION OF GAS: GENERAL IDEAS

The state of the solution is stipulated by temperature T, pressure Π and the initial concentration (the number density of molecules) n_0 of the dissolved gas. The meaning of value n_0 will be revealed further in the initial condition in Eq. (12) and in the boundary condition in Eq. (15). n_{∞} will stand for the concentration of the dissolved gas in the saturated solution, which at given temperature T and pressure Π is characterized by chemical and mechanical equilibrium with the clean gas above the plane contact surface. We shall consider the solution to be diluted. The solution contains a gas bubble (the same gas that is dissolved in the solution). Due to high heat conductivity of the liquid solvent, the bubble of gas will have the same temperature T as the solution does. The condition that the latter is valid and that the temperature in the bubble is homothermal will be justified in section V. There we shall also justify the mechanical equilibrium of the bubble and the solution. The radius of the bubble will be designated as R.

We shall suppose the radius R to be that large that the following strong inequalities are observed:

$$R\gg 2\sigma/\Pi,$$
 (1)

$$R \gg 4sD/\alpha_c v_T$$
. (2)

Here σ is the surface tension of the liquid solvent (in the case of a diluted solution), D is the diffusion coefficient of gas molecules in the liquid solvent, α_c is the condensation coefficient of a gas molecule at the virtual transition of gas molecules from the bubble and into the solution [1], v_T is a mean heat velocity of a gas molecule inside the bubble, s is the gas solubility that is defined as a dimensionless value via

$$s \equiv kT n_{\infty}/\Pi,\tag{3}$$

where k is the Boltzmann constant.

When Eq. (1) is observed, the influence of the Laplace forces on the bubble is rather small and the pressure of gas inside the bubble at its mechanical equilibrium with the solution

is equal to pressure Π of the solution. At the same time the gas inside the bubble can be considered perfect; therefore for gas concentration in the bubble, that is designated as n_g , we have

$$n_q = \Pi/kT,\tag{4}$$

so n_g is unambiguously defined by temperature T and pressure Π of the solution. Using Eq. (3), we can also rewrite Eq. (4) as

$$n_q = n_{\infty}/s. (5)$$

Due to Eq. (5) value s defined in Eq. (3) corresponds to the usual understanding of solubility, that is, a ratio (at given temperature and pressure) of the volume of gas to the volume of liquid that has dissolved this gas. Solubility s and value n_{∞} depend not only on temperature T and pressure Π , but also on the type of solvent and on the type of dissolved gas.

We shall neglect the fugacity of the liquid solvent and do so for the following reason: let P_{β} be the pressure of the saturated vapor of the solvent. If we have a look at the thermodynamic diagram, at temperature T and pressure Π of the solution the solvent will be found deep within the area of the steadiness of the liquid phase. For this reason $P_{\beta} \ll \Pi$, which, using concentration n_{β} of the saturated vapor of the liquid solvent, can be rewritten as $n_{\beta} \ll \Pi/kT$. From this and from Eq. (4) it follows that $n_{\beta} \ll n_g$. Thus the bubble consists mainly of gas; that is why the fugacity of the solvent can in fact be neglected.

As it was shown in [3], the strong inequality in Eq. (2) is the condition for the existence of the diffusion regime of bubble growth. Leaving a certain reserve, let us assume that

$$R_0 \sim 20 \max \left\{ \frac{2\sigma}{\Pi}, \frac{4sD}{\alpha_c v_T} \right\}.$$
 (6)

Eq. (6) evaluates value R_0 of the bubble radius, which is initial for the existence of conditions in both Eq. (1) and Eq. (2). Jointly with those, Eq. (4) and the diffusion regime of the bubble growth are also well observed. The largest of the two values given in braces in Eq. (6) is, as a rule, the value of $2\sigma/\Pi$.

Let us introduce characteristic time t_0 , at which the following initial condition on the radius of the bubble is observed:

$$R(t)|_{t=t_0} = R_0. (7)$$

Time t is calculated from the time of nucleation of the bubble that is growing irreversibly. From Eq. (7) and the meaning of value R_0 it can be seen that after time t_0 after the nucleation of the bubble Eq. (4) and the diffusion regime of bubble growth will be observed simultaneously. The larger R_0 , that is, the more precise is the observation of Eqs. (1) and (2), the larger t_0 .

The bubble perturbs the surrounding solution. Let us designate the concentration of the dissolved gas at distance r from the centre of the bubble at time t as n(r,t). If the growth regime of the bubble is a diffusion one, the evolution equation is observed

$$\frac{\partial n(r,t)}{\partial t} = D\Delta n(r,t) - \operatorname{div}\left[n(r,t)\vec{\mathbf{v}}(\vec{r},t)\right] \quad (t \geqslant t_0). \tag{8}$$

The first member in Eq. (8) accounts for the diffusion of gas molecules, while the second member stipulates it that this diffusion occurs against the background of the movement of liquid solvent caused by the movement of the surface of the bubble and by the incompressibility of the solvent. If we study the velocity of solvent movement designated in Eq. (8) as $\vec{v}(\vec{r},t)$ in the spherical system of co-ordinates with the reference point in the centre of the bubble, we shall see that it has only radial component $v_r(r,t)$, for which, as it is obvious, the following is valid:

$$v_r(r,t) = \frac{R^2(t)}{r^2} \frac{dR(t)}{dt}.$$
(9)

Using Eq.(9) and some well-known formulas of vector operations

$$\Delta f \equiv \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial f}{\partial r} \right), \quad \text{div} \vec{A} \equiv \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 A_r \right)$$
 (10)

let us rewrite the evolution equation from Eq. (8) as follows

$$\frac{\partial n(r,t)}{\partial t} = \frac{D}{r^2} \frac{\partial}{\partial r} \left[r^2 \frac{\partial n(r,t)}{\partial r} \right] - \frac{R^2(t)}{r^2} \frac{dR(t)}{dt} \frac{\partial n(r,t)}{\partial r} \qquad (t \geqslant t_0). \tag{11}$$

At all r > 0 we have the following initial condition on the homogeneity of the concentration profile of the dissolved gas at time t = 0 of the bubble nucleation:

$$n(r,t)|_{t=0} = n_0 (r > 0).$$
 (12)

This condition brings about value n_0 as the initial concentration of the dissolved gas. In a supersaturated solution it is observed that $n_0 > n_{\infty}$.

During the diffusion regime of the bubble growth we have an equilibrium boundary condition on the surface of the bubble:

$$n(r,t)|_{r=R(t)} = n_{\infty} \quad (t \geqslant t_0). \tag{13}$$

We shall neglect the dependence of the right side of Eq. (13) on the radius of the bubble when this radius is significant and conforms with the limitation from Eq. (1).

Let us impose a boundary condition of the absence of an external source of the dissolved gas:

$$r^2 \left. \frac{\partial n(r,t)}{\partial r} \right|_{r=\infty} = 0. \tag{14}$$

This condition means that the solution and the bubble in it are physically isolated.

In accordance with Eqs. (12) and (14) it is also true that

$$n(r,t)|_{r=\infty} = n_0. (15)$$

Due to physical isolation of the solution and the bubble in it, value n_0 also has the meaning of concentration of the dissolved gas at an infinite distance from the bubble; and this value is constant in time.

Each element of the surface of the bubble of radius R is moving with the velocity of the movement of the incompressible liquid solvent. Thus,

$$n_g \frac{dR(t)}{dt} = D \left. \frac{\partial n(r,t)}{\partial r} \right|_{r=R(t)} \qquad (t \geqslant t_0).$$
 (16)

Eq. (16) can be interpreted simply. It corresponds to the diffusion flux of the numbers of molecules through the surface of radius R (there is no convection flux due to mobility of this surface). The diffusion flux is spent on the change in the number of molecules of gas in the bubble (which at $t \geqslant t_0$, in concordance with the initial condition from Eq. (7), has constant concentration n_g of pure gas). As the sign of the derivative by r in Eq. (16) obviously corresponds with the sign of value $n_0 - n_\infty$, then, in the case of supersaturated solution, Eq. (16) leads to

$$dR/dt > 0 \qquad (t \geqslant t_0) \tag{17}$$

− i. e. leads to the growth of the bubble with time.

In order to specify the state of the solution one can use value ζ instead of value n_0 . Value ζ can be defined as

$$\zeta \equiv (n_0 - n_\infty)/n_\infty. \tag{18}$$

In a supersaturated solution, where $\zeta > 0$, value ζ will be referred to as the supersaturation of a solution.

II. SELF-SIMILARITY OF THE THEORY

Following [7], let us introduce a self-similar variable ρ having assumed that

$$\rho = \frac{r}{R(t)} \quad (\rho \geqslant 1). \tag{19}$$

We shall look for the solution n(r,t) of the evolution equation (11) in the form of $n(\rho)$ of one variable ρ :

$$n(r,t) = n(\rho). \tag{20}$$

Here and further, for the sake of simplicity, we shall not mention that ρ is changing within the limits of $\rho \geqslant 1$.

In accordance with Eqs. (19) and (20) we have

$$\frac{\partial n(r,t)}{\partial t} = -\frac{r}{R^2(t)} \frac{dR(t)}{dt} \frac{dn(\rho)}{d\rho},\tag{21}$$

$$\frac{\partial n(r,t)}{\partial r} = \frac{1}{R(t)} \frac{dn(\rho)}{d\rho}.$$
 (22)

From Eqs. (16) and (22) we have

$$\frac{dR(t)}{dt} = \frac{D}{R(t)n_g} \left. \frac{dn(\rho)}{d\rho} \right|_{\rho=1}. \quad (t \geqslant t_0). \tag{23}$$

Let us rewrite Eq. (23) as

$$\frac{dR(t)}{dt} = \frac{Db}{R(t)} \qquad (t \geqslant t_0) \tag{24}$$

or, equivalently, as

$$dR^2/dt = 2Db \quad (t \geqslant t_0), \tag{25}$$

where we introduce an important dimensionless parameter b using

$$b \equiv \frac{1}{n_g} \left. \frac{dn(\rho)}{d\rho} \right|_{\rho=1}.$$
 (26)

In accordance with Eq. (25), the derivative dR^2/dt does not depend on time: along the axis of variable R^2 the bubble is "moving" with the velocity that does not depend on time and on the size of the bubble.

Relative measure of inaccuracy of the self-similar velocity of the movement of the bubble 2Db in Eq. (25) is equal to the relative measure of inaccuracy of Eq. (4), which, in its turn, does not exceed value $2\sigma/R_0\Pi$, which can be easily obtained from the estimate from Eq. (6).

It is easy to make sure that, if we take Eqs. (19) – (22) and Eq. (24) into consideration, the evolution Eq. (11) turns into an ordinary differential equation for function $n(\rho)$ of the following type:

$$\frac{d^2n(\rho)}{d\rho^2} + \left[\frac{2}{\rho} + b\left(\rho - \frac{1}{\rho^2}\right)\right] \frac{dn(\rho)}{d\rho} = 0. \tag{27}$$

Integrating Eq. (27), obtaining a constant from the first integration using Eq. (26), and a constant from the second integration using the boundary condition from Eq. (13), formulated by virtue of Eqs. (19) and (20) as $n(\rho)|_{\rho=1}=n_{\infty}$, we have

$$n(\rho) = n_{\infty} + n_g b e^{3b/2} \int_1^{\rho} \frac{dx}{x^2} e^{-bx^2/2 - b/x}.$$
 (28)

The fact that Eqs. (27) and (28) refer only to times $t \ge t_0$ is not stipulated for the sake of simplicity. As it is obvious from Eqs. (19) and (20), a self-similar formula (28) complies with the boundary condition from Eq. (14), that is the absence of an external source of the dissolved gas.

In order to find parameter b using Eq. (28) and the boundary condition from Eq. (15) formulated by virtue of Eqs. (19) and (20) as $n(\rho)|_{\rho=\infty}=n_0$, we come up with the following transcendental equation:

$$a = be^{3b/2} \int_{1}^{\infty} \frac{dx}{x^2} e^{-bx^2/2 - b/x},$$
 (29)

where an important dimensionless parameter a is introduced using

$$a \equiv \frac{n_0 - n_\infty}{n_q}. (30)$$

In the case of a supersaturated solution, from Eq. (30) it follows that

$$a > 0. (31)$$

In accordance with Eqs. (5) and (18), we can rewrite Eq. (30) as:

$$a = s\zeta. (32)$$

In order that the integral in Eq. (29) should converge and, simultaneously, that the right part of Eq. (29) should be positive in concordance with Eq. (31), it is required that

$$b > 0. (33)$$

Eqs. (24) and (33) have the previous inequality (17) as a consequence.

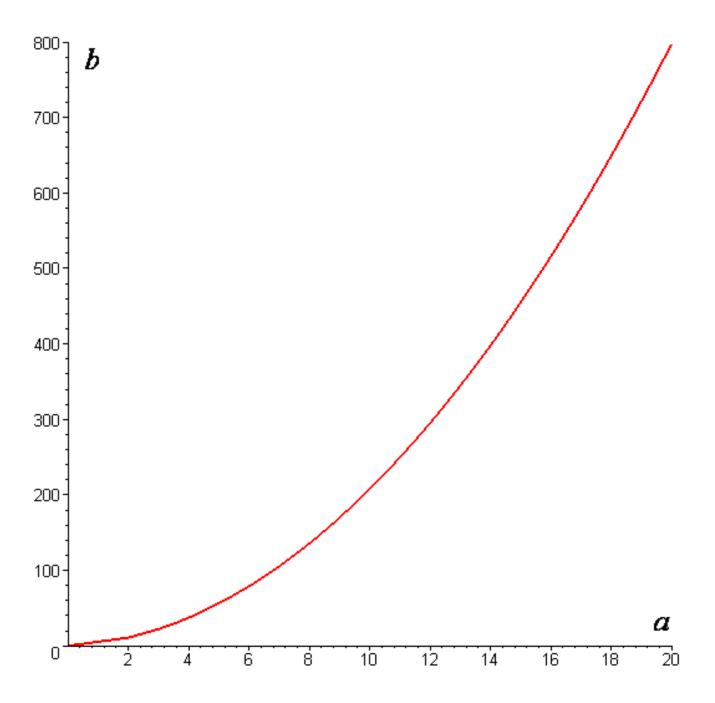


FIG. 1: Dependence of the solution b of Eq. (29) on parameter a.

Eq. (29) for b relative to a has an unambiguous solution within the area stipulated by Eq. (31). The results of numerical solution of Eq. (29) are represented by the curve in Fig. 1. This curve does not depend on the type of the solvent and on the type of the dissolved gas. All initial parameters of the problem are represented on the curve solely by means of parameter a introduced in Eq. (30).

Integrating Eq. (25) with the initial condition (7), we have

$$R^{2}(t) = 2Db \cdot (t - t_{0}) + R_{0}^{2} \quad (t \geqslant t_{0}). \tag{34}$$

When R_0 is significant, which is required by the estimate from Eq. (6), the relative measure of inaccuracy $2\sigma/R\Pi$ of the self-similar rate of bubble growth 2Db in Eq. (25) does not exceed 10% at times $t > t_0/4$ (and does not exceed 5% at times $t > t_0$). During the longest stage of the whole time interval $0 < t < t_0$, that is $t_0/4 < t < t_0$, the bubble, consequently, is growing practically with a self-similar rate 2Db. For this reason we can use an approximate formula

$$t_0 \simeq R_0^2 / 2Db, \tag{35}$$

where it is stipulated that the bubble is growing with a self-similar rate 2Db throughout the whole interval of $0 < t < t_0$. From Eqs. (34) and (35) we have

$$R^2(t) \simeq 2Db \ t \quad (t \geqslant t_0), \tag{36}$$

which makes it possible to find R(t) in Eq. (19) at all times $t \ge t_0$. The larger R_0 , the more accurate Eqs. (35) and (36) are.

Let us now explicitly formulate the sequence in which the values that are found during an experiment are introduced within the theory. The state of the solution is given by its temperature T, pressure Π and the initial concentration n_0 of the dissolved gas (introduced into the theory by means of the initial condition in Eq. (1.12)). Using the given T and Π one can obtain from an experiment (at a stipulated type of solvent and type of a dissolved gas) value n_{∞} , and, knowing T, Π and n_{∞} , using definition from Eq. (3), we introduce the theory with gas solubility s. Then, using either of Eqs. (4) or (5), we obtain value n_g (that is unambiguously defined by temperature T and pressure Π). Finally, knowing n_0 , n_{∞} and n_g , by means of definition from Eq. (30) we introduce value a.

It should be mentioned that in order to stipulate value n_0 in the experiment it is convenient to proceed from saturated solution at pressure that is larger than pressure Π that is of interest to us. Let us identify value n_{∞} obtained during the experiment with value n_0 , and then instantly reduce the pressure in the solution to Π . Due to low compressibility of the liquid solvent, the solution will become just what we are interested in – supersaturated solution with the given concentration n_0 of the dissolved gas.

III. DEPENDENCE OF THE BUBBLE GROWTH RATE ON GAS SOLUBILITY AND SOLUTION SUPERSATURATION

In accordance with section II, self-similar Eq. (29) defines parameter b as an unambiguous function b = b(a) of parameter a throughout all the area stipulated by Eq. (31). Function b = b(a) does not depend on the type of the solvent and on the type of the dissolved gas. Having multiplied function b = b(a) by 2D, using self-similar Eq. (25), we have the following equality

$$dR^2/dt = 2Db(a) (t \geqslant t_0) (37)$$

for the constant in time derivative dR^2/dt , which characterizes the rate of bubble growth (the rate of the growth of its surface). Function b = b(a), which was obtained via numerical solution of the self-similar Eq. (29), is just what is presented in Fig. 1. It can be seen that with the increase of parameter a in the area stipulated by Eq. (31) this function is growing faster than parameter a is.

The physical meaning of parameter a is revealed in Eq. (32). Exploiting this in Eq. (37), we have

$$dR^2/dt = 2Db(s\zeta) \quad (t \geqslant t_0). \tag{38}$$

Eq. (38) shows that derivative dR^2/dt is proportional to diffusion coefficient D of the molecules of gas in the solution and depends on the solubility of the gas s and solution supersaturation ζ only via the product of $s\zeta$. Curve 1 in Fig. 2 represents data concerning the dependence of dimensionless value $D^{-1}dR^2/dt$ on $s\zeta$ obtained by means of Eq. (38) and the numerical solution of the self-similar Eq. (29). It is clear that with the increase of $s\zeta$ from $s\zeta = 0,01$ to $s\zeta = 20$, value $D^{-1}dR^2/dt$ is growing at an increasing rate from $D^{-1}dR^2/dt = 2 \cdot 10^{-2}$ to $D^{-1}dR^2/dt = 1,5 \cdot 10^3$. The revealed effect of the significant increase of the rate of bubble growth simultaneous with the increase in the product of gas solubility s and solution supersaturation ζ is nonsteady by its virtue; and this will be shown in section IV.

When $a \gtrsim 10$, the solution of the self-similar Eq. (29) can be found analytically. Let us rewrite this equation as

$$\frac{a}{b} = \int_{1}^{\infty} \frac{dx}{x^2} \exp\left(-\frac{bx^2}{2} - \frac{b}{x} + \frac{3b}{2}\right). \tag{39}$$

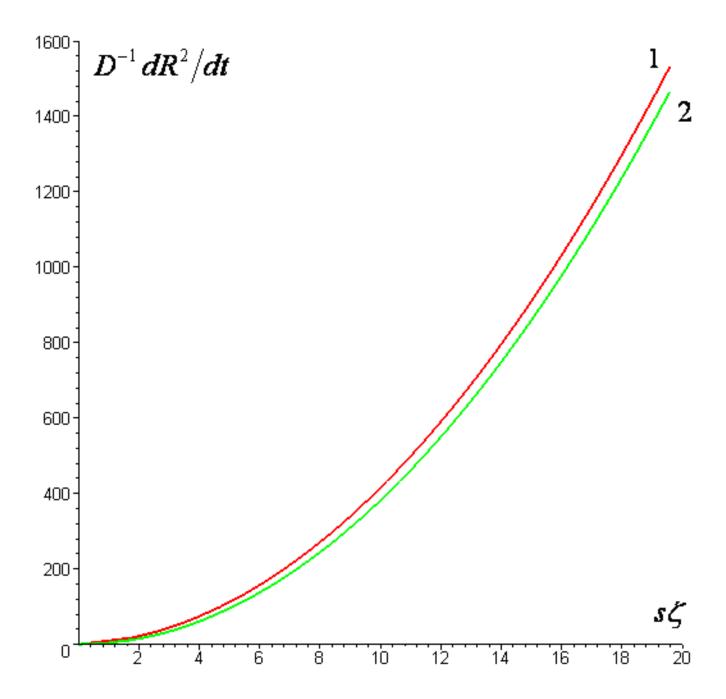


FIG. 2: Dependence of dimensionless value $D^{-1}dR^2/dt$ on the product $s\zeta$.

Expanding the exponent from Eq. (39) into a Taylor series in powers of x-1 in the vicinity of x=1, noting that at $b\gg 1$ the exponent "cuts" the integral in Eq. (39) already before $1/x^2$ manages to practically deviate from unit, using saddle-points technique, we have

$$\int_{1}^{\infty} \frac{dx}{x^2} \exp\left(-\frac{bx^2}{2} - \frac{b}{x} + \frac{3b}{2}\right) = \left(\frac{\pi}{6}\right)^{1/2} b^{-1/2} \quad (b \gtrsim 2 \cdot 10^2). \tag{40}$$

Substituting Eq. (40) in Eq. (39), we come up with an analytical solution of the self-similar

Eq. (29):

$$b(a) = \frac{6}{\pi}a^2 \quad (a \gtrsim 10). \tag{41}$$

Eq. (41) at the limit of its applicability $a \approx 10$ concords well with the graph given in Fig. 1. Thus analytical Eq. (41) conjointly with Fig. 1 provides comprehensive data on function b = b(a) throughout all the area stipulated by Eq. (31). Curve 2 in Fig. 2 represents data on the dependence of dimensionless value $D^{-1}dR^2/dt$ on $s\zeta$ obtained by means of Eq. (38) and the analytical Eq. (41).

Exploiting Eq. (41) in Eq. (38), we have

$$\frac{dR^2}{dt} = \frac{12D}{\pi} (s\zeta)^2 \quad (s\zeta \gtrsim 10, \ t \geqslant t_0). \tag{42}$$

Analytical formula (42) shows that the derivative dR^2/dt is growing rather quickly with the growth of $s\zeta$ at $s\zeta\gtrsim 10$.

Let us assess time t_0 in the condition $t \ge t_0$ of the applicability of Eqs. (37), (38) and (42). Let us rewrite t_0 in accordance with Eqs. (35) and (25) as

$$t_0 \simeq R_0^2 / (dR^2 / dt). \tag{43}$$

Eq. (43) shows that value represents the rate of relative increase of the area of the bubble surface at time t_0 .

For radius R_0 introduced by means of Eq. (6), let us write

$$R_0 \sim 40 \frac{\sigma}{\Pi},\tag{44}$$

where it is considered that the largest of the two values given in braces in Eq. (6) is, as a rule, value $2\sigma/\Pi$. In accordance with Eq. (44), relative deviation of pressure in the bubble of radius $R \geqslant R_0$ from pressure Π of the solution does not exceed 5%. Let us assume that $\Pi \simeq 10^6 \frac{\text{dyne}}{\text{cm}^2} \simeq 1$ atm and $\sigma \simeq 75 \frac{\text{dyne}}{\text{cm}}$ (as in case of water). Then, from Eq. (44) we have

$$R_0 \sim 3 \cdot 10^{-3} \text{ cm.}$$
 (45)

Let us find the derivative dR^2/dt in Eq. (43) by means of Fig. 2, using the value that is typical for water: $D \simeq 1, 6 \cdot 10^{-5} \frac{\text{cm}^2}{\text{s}}$ [8]. Further we shall obtain R_0^2 in Eq. (43) using the evaluation from Eq. (45). The data on the dependence of the evaluation of time t_0 on $s\zeta$ obtained in the described way are presented in Fig. 3.

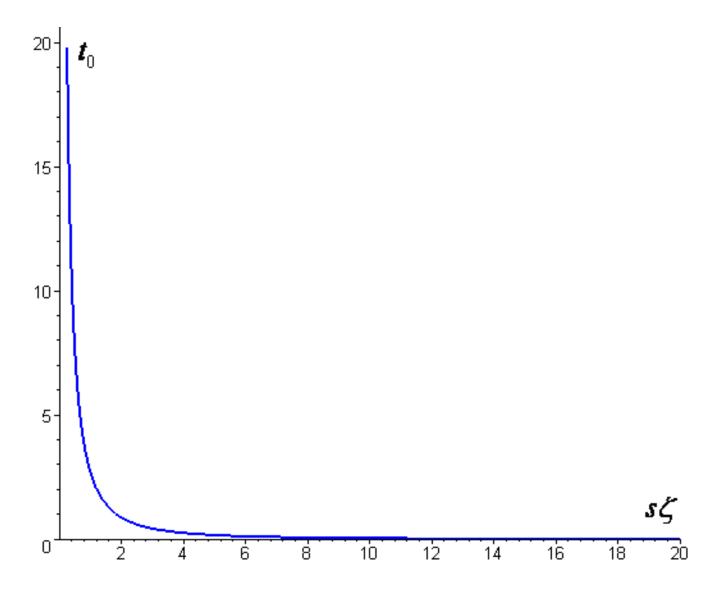


FIG. 3: Dependence of the estimation for the time t_0 (s) on the product $s\zeta$.

Using the analytical Eq. (42) in Eq. (43) at the same value of diffusion coefficient D and the same evaluation from Eq. (45), we have

$$t_0 \sim \frac{1, 5 \cdot 10^{-1}}{(s\zeta)^2} \,\mathrm{s} \quad (s\zeta \gtrsim 10).$$
 (46)

Analytical Eq. (46) and Fig. 3 provide exhaustive data on the evaluation of time t_0 throughout all the area of $s\zeta > 0$.

Let us notice that the Eq. (36) can be rewritten using Eq. (35) as

$$R^2(t) \simeq R_0^2 t/t_0 \quad (t \geqslant t_0),$$
 (47)

where values R_0 and t_0 evaluated previously are present.

IV. STEADY THEORY CASE

Let us study a case when

$$(s\zeta)^{1/2} \ll 1. \tag{48}$$

Thus, from Eq. (32) it follows that

$$a^{1/2} \ll 1.$$
 (49)

As we shall see further, inequality in Eq. (49) will help us to solve a self-similar Eq. (29) analytically. The same inequality will also stipulate the range of applicability of the steady theory.

Let us begin by solving Eq. (29). Differentiating by b, one can make sure that the following asymptotic equation is observed:

$$\int_{1}^{\infty} \frac{dx}{x^2} e^{-bx^2/2 - b/x} = 1 - \left(\frac{\pi}{2}\right)^{1/2} b^{1/2} + \dots \quad (b^{1/2} \ll 1), \tag{50}$$

where the neglected components in terms of their value are even smaller than b. Using Eq. (50) in a self-similar Eq. (29), considering only its main component, we shall have a = b, which, by virtue of Eq. (49), confirms the condition $b^{1/2} \ll 1$ in Eq. (50). As a result, the solution of a self-similar Eq. (29), in case when Eq. (49) is observed, in the principal order by $a^{1/2}$ looks as follows:

$$b = a (a^{1/2} \ll 1). (51)$$

Now let us define the range of applicability of the steady theory. Let us substitute Eq. (51) in the self-similar Eq. (28). Thus we have

$$n(\rho) = n_{\infty} + n_g a \int_1^{\rho} \frac{dx}{x^2} \exp\left(-\frac{ax^2}{2} - \frac{a}{x} + \frac{3a}{2}\right) \qquad (a^{1/2} \ll 1).$$
 (52)

Let us prove that the concentration profile of the dissolved gas in Eq. (52), which was obtained at the limitation from above on a expressed in Eq. (49), is steady in the area of

$$1 \le \rho \lesssim 2^{1/2} / 4a^{1/2} \quad (a^{1/2} \ll 1),$$
 (53)

that exists simultaneously with limitation from Eq. (49). In the area stipulated by Eq. (53) the absolute value in the exponent in Eq. (52) is rather small (smaller than 1/16), and the exponent itself, consequently, is rather close to 1. Taking this fact into consideration and

also developing a in the multiplier in front of the integral in Eq. (52), using definition from Eq. (30), in the area stipulated by Eq. (53) we shall with high precision deduce Eq. (52) to

$$n(\rho) = n_0 - \frac{n_0 - n_\infty}{\rho} \quad (a^{1/2} \ll 1, \quad 1 \leqslant \rho \lesssim 2^{1/2} / 4a^{1/2}).$$
 (54)

Eq. (54) corresponds to the steady concentration profile of the dissolved gas. We also provide limitations on a and on ρ ; when those limitations are observed Eq. (54) stems from a general self-similar Eq. (28) for the nonsteady concentration profile of the dissolved gas.

In order to find the rate of bubble growth, as it can be seen from Eq. (23), it is enough to know the derivative $dn(\rho)/d\rho|_{\rho=1}$, i.e. it is enough to know the concentration profile of the dissolved gas only in the infinitely narrow vicinity of the bubble. But even then one can obtain this data within the framework of the steady approximation of Eq. (54) only when the limitation Eq. (49) is observed. Indeed, already when $a^{1/2} \gtrsim 2^{1/2}/4$ (when the limitation of Eq. (4.2) is no longer observed) the area stipulated by Eq. (53) does not exist at all; and, consequently, there is no such thing as an infinitely narrow vicinity of the bubble, where the concentration profile of the dissolved gas could be steady.

We see that the limitation in Eq. (49) is necessary for works [1, 2, 3, 4, 5, 6] based on the steady theory and devoted to the study of bubble growth. At the same time, it becomes clear that the rapid increase in the rate of bubble growth, which, as it was revealed in section III, occurs at the increase of the product $s\zeta$, and, consequently, at the increase of value a(when Eq. (4.2) is not observed), is of a significantly nonsteady nature.

Finally, let us apply the analytical solution from Eq. (51) of the self-similar Eq. (29) to the problem of finding the rate of bubble growth. Substituting Eq. (51) in the self-similar Eq. (25), we have

$$dR^2/dt = 2Da (a^{1/2} \ll 1) (55)$$

(for the sake of simplicity we do not point out the inequality $t \ge t_0$ which is the condition for the observation of Eq. (25)). Exploiting Eq. (32) in Eq. (55), we have

$$dR^2/dt = 2Ds\zeta \quad ((s\zeta)^{1/2} \ll 1). \tag{56}$$

Using the definition from Eq. (3), Eq. (56) can be rewritten as

$$\frac{dR}{dt} = \frac{kTn_{\infty}D}{R\Pi}\zeta. \tag{57}$$

Under the condition that $P_{\beta} \ll \Pi$ specified in the beginning of section I, Eq. (57) coincides with Eq. (2.7) in [4] obtained at low gas solubility.

V. RANGE OF APPLICABILITY OF THE THEORY

Let us first find the condition on the smallness of the deviation of the bubble temperature from the temperature of the solution. The transition of a molecule of gas from the solution to the bubble, as a rule, occurs with absorption of heat. As a result, the temperature of the bubble, which we will denote as T_g , becomes smaller than temperature T of the solution (now we perceive T as the temperature of the solution at the infinite distance from the bubble). In order to find the deviation $T_g - T$, one preliminary has to find the nonsteady temperature profile T(r,t) around the bubble by solving the heat conductivity equation in the liquid solvent moving outside the bubble with the boundary condition $T(r,t)|_{r=\infty} = T$ and at the intensity of absorption of heat by the bubble stipulated by the rate of its growth. This can be achieved, just as in section II, by means of a self-similar method based on the substitution $T(r,t) = T(\rho)$, where a self-similar variable ρ is given by the previously used equality (19). (Study of nonsteady heat conductivity problem is important for the growth of a liquid droplet in supersaturated vapor [9]). Using this method and obtaining $T(\rho)$, we will have the following equality for the unknown deviation $T_g - T$, where T_g is defined as $T_g \equiv T(\rho)|_{\rho=1}$:

$$T_g - T = -\frac{qDn_g}{\kappa}b \int_1^\infty \frac{dx}{x^2} \exp\left(-\frac{\varepsilon bx^2}{2} - \frac{\varepsilon b}{x} + \frac{3\varepsilon b}{2}\right). \tag{58}$$

Here q is the heat of dissolution per one molecule of gas (as a rule, q > 0), κ is the coefficient of heat conductivity of the liquid solvent in the diluted solution,

$$\varepsilon \equiv D/\chi,\tag{59}$$

 χ is the coefficient of thermal diffusivity of the liquid solvent in the diluted solution. For the rate of bubble growth in Eq. (58) we have used Eq. (25), which is enough to assert the smallness of heat effect, (but not enough to study it).

Replacing value b with value εb in Eq. (40), we have

$$\int_{1}^{\infty} \frac{dx}{x^2} \exp\left(-\frac{\varepsilon bx^2}{2} - \frac{\varepsilon b}{x} + \frac{3\varepsilon b}{2}\right) = \left(\frac{\pi}{6}\right)^{1/2} (\varepsilon b)^{-1/2} \quad (\varepsilon b \gtrsim 2 \cdot 10^2). \tag{60}$$

From Eqs. (58) and (60) we have

$$T_g - T = -\frac{qDn_g}{\varepsilon^{1/2}\kappa} \left(\frac{\pi}{6}\right)^{1/2} b^{1/2} \quad (b \gtrsim 2 \cdot 10^2/\varepsilon). \tag{61}$$

We shall assume values characteristic for water in ordinary conditions [8]:

$$D \simeq 1, 6 \cdot 10^{-5} \frac{\text{cm}^2}{\text{s}}, \quad \kappa \simeq 6 \cdot 10^4 \frac{\text{erg}}{\text{cm} \times \text{s} \times \text{K}}, \quad \chi \simeq 1, 4 \cdot 10^{-3} \frac{\text{cm}^2}{\text{s}}.$$
 (62)

Then, for value ε introduced in Eq. (59) we have

$$\varepsilon \simeq 10^{-2}$$
. (63)

As can be seen from Eqs. (41) and (63), limitation $b \gtrsim 2 \cdot 10^2/\varepsilon$ in Eq. (61) is equipotent to limitation $a \gtrsim 10^2$ which makes Eq. (41) correct. Then, in accordance with Eqs. (61), (63) and (41), we have

$$T_g - T \simeq -\frac{10qDn_g}{\kappa} a \qquad (a \gtrsim 10^2). \tag{64}$$

Using Eq. (64) we have

$$\frac{|T_g - T|}{T} \simeq \frac{10|q|Dn_g}{\kappa T} a \qquad (a \gtrsim 10^2). \tag{65}$$

Let us accept that

$$\Pi \simeq 10^6 \frac{\text{dyne}}{\text{cm}^2}, \quad T_g \simeq 300 \text{ K}, \quad |q|/kT \simeq 10.$$
 (66)

We will use Eqs. (62), (66) in Eq. (65), and then expand n_g by means of Eq. (4). Thus we will have

$$|T_q - T|/T \simeq 10^{-4}a \quad (a \gtrsim 10^2).$$
 (67)

From Eq. (67) it follows that

$$|T_g - T|/T \lesssim 10^{-1}$$
 when $a \lesssim 10^3$, (68)

where we do not refer to limitation $a \gtrsim 10^2$ in Eq. (67), as in accordance with physical meaning the value in the left part of Eq. (68) decreases with the decrease of value a. Inequality in Eq. (68) reveals the smallness of the relative deviation of the bubble temperature from the temperature of the solution even in the case of very large values of parameter $a = s\zeta \lesssim 10^3$, where Eq.(32) is observed.

Now we will obtain the condition on the equalization of the temperature of the bubble. For time t_g which is characteristic for this equalization we have the following estimate: $t_g \sim R^2/\chi_g$, where χ_g is the coefficient of thermal diffusivity of gas in the bubble. Let us now introduce characteristic time $t_R = R/(dR/dt)$ for the changing of the bubble radius. The fact that the temperature of the bubble manages to establish in the process of the bubble growth is equivalent to strong inequality $t_g \ll t_R$, that is

$$R/\chi_q \ll 1/(dR/dt). \tag{69}$$

By means of self-similar Eq. (24) we shall rewrite Eq. (69) as

$$Db/\chi_g \ll 1. \tag{70}$$

Using Eq. (41), we have

$$\frac{Db}{\chi_q} = \frac{6}{\pi} \frac{D}{\chi_q} a^2 \qquad (a \gtrsim 10). \tag{71}$$

From Eq. (71), taking Eq. (62) and the fact that $\chi_g \sim 10^{-1} \frac{\text{cm}^2}{\text{s}}$ into consideration, it follows that

$$Db/\chi_g \lesssim 10^{-1} \text{ when } a \lesssim 1, 8 \cdot 10,$$
 (72)

where we do not refer to limitation $a \gtrsim 10$ in Eq. (71), as value b decreases with the decrease of value a. Inequality in Eq. (72) reveals the smallness of value Db/χ_g in the condition from Eq. (70) at all values of $s\zeta \lesssim 1, 8 \cdot 10$, where Eq.(32) is observed.

Thus, if we consider conditions on the isothermal character of the bubble growth in Eqs. (68) and (72), the latter condition turns out to be stronger, that is

$$s\zeta \lesssim 1, 8 \cdot 10. \tag{73}$$

Still it leaves broad possibilities for the application of the isothermal theory. Indeed, the condition from Eq. (73) in accordance with Eq. (42) admits even that

$$0 < D^{-1}dR^2/dt \lesssim 1, 2 \cdot 10^3 \qquad (s\zeta \lesssim 1, 8 \cdot 10, \ t \geqslant t_0), \tag{74}$$

where the limitation $s\zeta \gtrsim 10$ in Eq. (42) is not mentioned as $D^{-1}dR^2/dt$ decreases with the decrease of $s\zeta$. As for velocity $1/t_0$ of the relative increase of the area of the bubble surface at time t_0 , the condition in Eq. (73) in accordance with Eq. (46) admits even that

$$0 < 1/t_0 \lesssim 2, 3 \cdot 10^3 \,\mathrm{s}^{-1} \qquad (s\zeta \lesssim 1, 8 \cdot 10), \tag{75}$$

where limitation $s\zeta\gtrsim 10$ in Eq. (46) is not mentioned as $1/t_0$ decreases with the decrease of $s\zeta$. The ranges of alteration of values $D^{-1}dR^2/dt$ $1/t_0$ (74) (75) comprise three orders of magnitude. Therefore, the possibilities of the isothermal theory are rather broad.

Let us prove that the observation of the condition from Eq. (73) causes the observation of the condition on the diluteness of the solvent. In accordance with Eqs. (4), (5) and (18), we have

$$n_0 = (s\zeta + s)\Pi/kT. \tag{76}$$

As $s \ll 10$ is correct in all cases, then from Eq. (76) in accordance with Eq. (66) it follows that

$$n_0 \lesssim 4, 3 \cdot 10^{20} \text{ cm}^{-3} \qquad (s\zeta \lesssim 1, 8 \cdot 10).$$
 (77)

The estimation from Eq. (77) shows that, when the condition in Eq. (73) is observed, the concentration n_0 of the dissolved gas is approximately two orders less that the concentration n_l of the liquid solvent $(n_l \simeq 3 \cdot 10^{22} \text{ cm}^{-3} \text{ for the case of water})$. This substantiates the diluteness of the solvent.

Let us finally find the condition which is responsible for the observation of the mechanical equilibrium of the bubble and the solvent which was presupposed in the paper. We will use t_h to denote the time of mechanical relaxation of the bubble under the influence of the hydrodynamic interaction between the bubble and the solvent. As we consider large bubbles, i. e. cases when, in accordance with the estimation in Eq. (45), $R \gtrsim 3 \cdot 10^{-3}$ cm, the following inequality is observed

$$3\Pi \rho_p R^2 / 4\eta^2 > 1, (78)$$

where ρ_p and η are mass density and the viscosity of the solvent accordingly. Indeed, this fact is obvious from $\Pi \simeq 10^6 \frac{\text{dyne}}{\text{cm}^2}$, $\rho_p = 1 \frac{\text{g}}{\text{cm}^3}$ and $\eta = 10^{-2} \frac{\text{g}}{\text{cm} \times \text{s}}$. As it has been shown in [2], when inequality in Eq. (78) is observed, the mechanical relaxation of the bubble is of oscillation and attenuation character, while time t_h of this relaxation is given by the following equality:

$$t_h = \rho_p R^2 / 2\eta \tag{79}$$

(Eq. (23) in [2]). Let us introduce characteristic time $t_R = R/(dR/dt)$ of the alteration of the radius of the bubble. The condition on the observation of the mechanical equilibrium of the bubble and the solvent is

$$t_h/t_R \ll 1. \tag{80}$$

Obtaining t_R by means of Eq. (42) and taking Eq. (79) into account, we have

$$\frac{t_h}{t_R} = \frac{3\rho_p D}{\pi \eta} (s\zeta)^2 \qquad (s\zeta \gtrsim 10). \tag{81}$$

From Eq. (81), when $D \simeq 1, 6 \cdot 10^{-5} \frac{\text{cm}^2}{\text{s}}, \rho_p = 1 \frac{\text{g}}{\text{cm}^3}$ and $\eta = 10^{-2} \frac{\text{g}}{\text{cm} \times \text{s}}$

$$t_h/t_R < 5 \cdot 10^{-1} \quad (s\zeta \lesssim 1, 8 \cdot 10),$$
 (82)

where we do not point at limitation $s\zeta \gtrsim 10$ in Eq. (81), as in accordance with physical meaning value t_h/t_R decreases with the decrease of value $s\zeta$. In accordance with Eq. (82), the inequality in Eq. (80) is observed in the vicinity of the boundary value even under the condition of Eq. (73) which, as it has been mentioned earlier provided extensive possibilities for the application of the theory. We will impose this condition on $s\zeta$ in Eq. (82) in order to reveal it that the mechanical equilibrium between the bubble and the solvent and the equalization of temperature inside the bubble cease being observed at approximately the same values of $s\zeta$.

In conclusion we will note that the smallness of gas solubility was not exploited in the present paper.

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